

Removal of Lead from Waste Water using Lantana Camara as Adsorbent



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Abstract: As we are moving towards the development by urbanization and industrialization on the other hand it is becoming a major environmental impact. Due to the urbanization and industrialization, many processing industries causing major environmental problem, among these problems heavy metal pollution by allowing of industrial waste water into natural water bodies is more dreadful. This is turn increase the heavy metal concentration in natural water bodies resulting in damage to aquatic flora and fauna. The objective of this study is to determine the heavy metal concentration (i.e. Pb) in industrial waste water, in this project waste water from one of the electroplating industries in Bangalore; this study gives knowledge about the percentage removal of lead using lantana camara as an adsorbent. The optimum condition for effective removal of lead is studied by conducting various experiments by varying adsorbent dosage and agitation time and by plotting isotherms, i.e. langmuir isotherms and Freundlich isotherms and pseudo I order and pseudo II order kinematics. This study is carried out using spectrophotometer analysis.

Keywords - adsorbent, adsorbate, adsorbtion, isotherms, kinetics, lead, absorbance.

I. INTRODUCTION

Environmental heavy metal pollution is mainly of anthropogenic in nature and results from activities such as vehicular emission, industrial activities, fertilizers draining into rivers, sewage and municipal waste etc. Certain plants like lantana camara and commelina benghalensis are good adsorbent in nature after some processing. In this project lantana camara is used as adsorbent for removal of lead, earlier experiments were conducted using lantana camara for removal of other heavy metals such as copper, cadmium, zinc, etc. Lead is of particular interest, because of its toxicity and its widespread presence in environment and it is considered as prior pollutant. Lead may enter water bodies both naturally and can also be induced. Natural source are volcanos, forest fire, weathering of rocks etc., where as it is induced into environment by human activities such as industries, combustion in vehicles, waste management etc. Lead has its adverse effect on both human health and aquatic ecosystem. Lead has adverse behavioral, psychological effect

on humans, where as it leads to bio concentration in skin, bones, kidneys, liver of fishes leading to disturbance in aquatic system. Lead can be removed precipitation, ion exchange, electro-coagulation, cementation, reverse osmosis and adsorption method. In this project adsorption method was selected due to its increased interest and its an alternative for high cost, sensitive conventional technologies. In this project Lantana camara is used as adsorbent due to its property such as hyper accumulation, natural availability and inexpensive. The variations were made in adsorption dosage, agitation time and optimum condition for removal of lead was determined and Freundlich and Langmuir isotherms were drawn along with pseudo I and II order isotherms. This analysis was made using UV spectrophotometer.

II. MATERIAL AND METHODOLOGY

A. Material

Lantana camara (Adsorbent): Lantana camara is a species of flowering plant within the verbena family, plant species accumulates significant amount of the some heavy metals .These plants are hyper accumulative and can be obtained naturally hence it can be effectively used as an inexpensive adsorbent for removal of lead from industrial waste water.

B. Equipments

The equipment's used in this study for different experiment are pH meter, naphelo turbidity meter, weighing balance, uv spectrophotometer, furnace, hot air oven and water bath.

C. Methodology

- Collection of lantana camara sample from agricultural site in Coorg, it is powdered and crushed to smaller size. Particle passing through 0.030mm are collected.
- Crushed particle is activated using con Sulphuric acid for better adsorption, heated at 120oC for 12 hours in furnace then double washed with distilled water and dried in hot air oven for 5 hours at 130oC. The dried sample is sieved and particles passing through .030mm and retained over .015mm are collected due to availability of larger surface area.
- Collection of industrial waste water from electroplating industry located in Bangalore.
- Preliminary test on collected sample.
- Modeling analysis of sample by varying adsorbent dosage and agitation time.
- Water sample is tested for percentage removal of lead using spectrophotometer.

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- Test result are tabulated and analyzed using isotherms and kinematics.

III. TEST RESULT

A. Preliminary Test Results

- Preliminary Test Results
- pH of collected sample from pH meter was 8.76 and the result from pH paper was 9. The pH value signifies that sample is alkaline in nature.
- Phenol alkalinity of sample was calculated and found out to be 9.5mg/lit, where as methyl orange alkalinity was found out to be 40.6mg/lit.
- Available chloride in sample was 18.25 mg/lit.
- Total hardness of industrial waste water was 86mg/lit.
- Total solids were measured to be 2600mg/lit, dissolved solids was found out to be 1066.67mg/lit, whereas the amount of suspended solids was 1533.33mg/lit.
- The collected water sample was 17.7NTU turbid.

B. Result of absorbance for various adsorption dosage

The variation of absorbance with respect to dosage is tabulated in table 1 and graphically represented in figure 1

C. Result of absorbance for varying agitation time

The variation of absorbance with respect to agitation time is tabulated in table 2 and graphically represented in figure 2.

D. Langmuir isotherms

The expression for Langmuir isotherm is given below

$$1/q_e = 1/(q_m K_L) (1/C_e) + 1/q_m$$

Where

q_e = amount of solute adsorbed per unit weight of the adsorbent at equilibrium (mg/g)

q_m = the maximum adsorption capacity (mg/g)

C_e = the equilibrium concentration of the solute in the bulk solution (mg/L)

K_L = Langmuir constant.

In terms of a dimensionless equilibrium parameter (RL) the essential characteristics of Langmuir isotherm can be expressed

$$R_L = 1 / (1 + K_L C_0)$$

Where,

K_L = Langmuir constant,

C_0 = Initial concentration (mg/L).

The type of the isotherm is indicated from the value of R_L .

If $R_L > 1$: Unfavorable: $R_L = 1$: Linear: $0 < R_L < 1$:

Favorable: $R_L = 0$: Irreversible.

The data for Langmuir isotherm for various dosage and agitation time and represented in fig 3 and fig 4 respectively

E. Freundlich isotherm

The expression for Langmuir isotherm is given below

$$\log q_e = (\log K + 1/n) \log C_e$$

where,

q_e = amount of solute adsorbed per unit weight of the adsorbent at equilibrium (mg/g)

C_e = the equilibrium concentration of the solute in the bulk solution (mg/L)

K_F and n = Freundlich Isotherm.

Adsorption intensity is measured by the slope $1/n$ ranging between 0 and 1.

As the $1/n$ value gets closer to zero, it becomes more heterogeneous.

A value of $1/n$ below one indicates unfavorable condition.

$1/n$ above one is indicative of favorable condition.

The data for Freundlich isotherm for various dosage and agitation time represented in fig 4. And fig 5 respectively.

F. Pseudo I and II order kinematics

The pseudo I orders and pseudo II order expression are given below and they are represented in fig 6 and fig 7 respectively.

$(q_e - q_t) = \log q_e - K_1/2.303 t$ pseudo I order kinematics

$t/q_t = 1/(K_2 q_e^2) + 1/q_e t$ pseudo II order kinematics

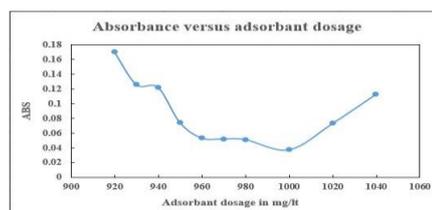


Figure 1 Absorbance variation with dosage

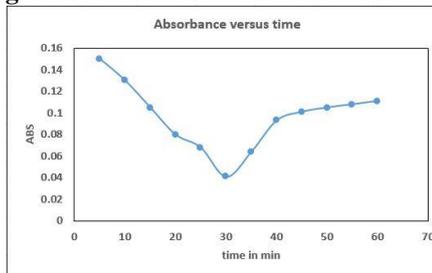


Figure 2 Absorbance variation with time of agitation

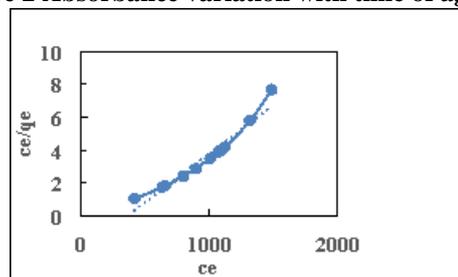


Figure 3 Langmuir isotherm for varying dosage

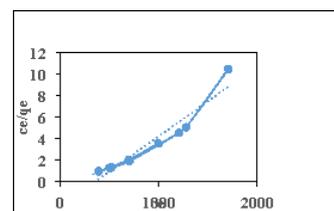
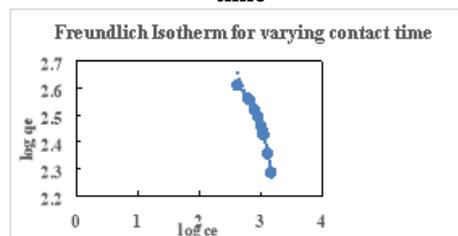


Figure 4 Langmuir isotherm for varying agitation time



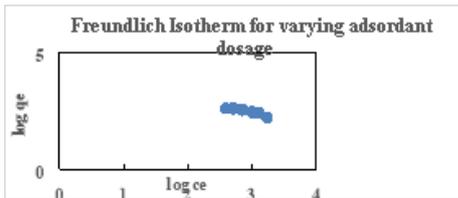


Figure 5 Freundlich Isotherm For Varying Dosage

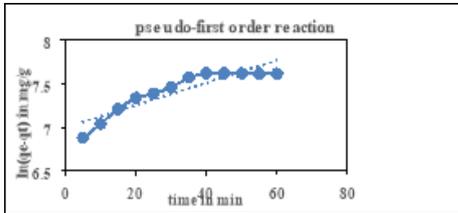


Figure 6 Pseudo first order

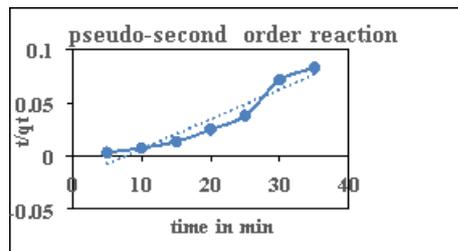


Figure 7 Pseudo second order

IV. CONCLUSION

Variation of Adsorbant dosage

Adsorbent dosage takes 920, 930, 940, 950, 960, 970, 980, 1000, 1020 and 1040mg/lit.

Optimum dosage obtained: 1000mg/lit.

Initial concentration of waste water sample=2460mg/lit.

After adsorption process by 1000mg/lit of adsorbent concentration of the sample =390 mg/lit.

Percentage removal of lead = $\frac{(2460-390)}{2460} \times 100 = 84.15\%$

Variation of Contact Time

Time: 5,10,15,20,25,30,35,40,45,50,55 and 60 min.

Optimum: 30 min.

Adsorbent dosage: 1000mg/lit

After adsorption process for 30 min by 1000mg/lit of adsorbent concentration of the sample =420 mg/lit.

Percentage removal of lead = $\frac{(2460-420)}{2460} \times 100 = 82.92\%$

From the results of batch adsorption kinetic study, shows that pseudo – second order kinetic model provided a good correlation for adsorption of lead from industrial waste water sample. The results of batch adsorption data for Langumir, Freundlich isotherm plots indicated that Langumir adsorption isotherm fitted well for adsorption of lead on Lantana camara sample as an adsorbent.

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