

Experimental Study of Heat Transfer Rate in Single and Series Cross Flow Heat Exchanger using Matlab Coding



P.ParabrahmaSai, K.Lakshmi Prasad, P.Ravindra Kumar, K. Srinivasa Rao

Abstract: The present study investigates the heat transfer rate and effectiveness of cross flow heat exchanger by varying velocity and mass flow rate of the cold and hot fluids. The velocity of the cold fluid i.e. air varying from 15m/s to 30m/s (with an intermediate step of 20m/s and 25m/s) whereas the mass flow rate of hot fluid i.e. water is taken as 35lit/hr and 84lit/hr. The logarithmic mean temperature difference (LMTD) method is used to find the heat transfer rate. In the present work the effectiveness and heat transfer rate were compared between the single and series cross flow heat exchangers. The result shows an average increase of 47.14% and 59.59% of heat transfer rate analogous to mass flow rate of 84lit/hr and 35lit/hr.

Keywords: Cross flow Heat exchanger, Effectiveness, Heat transfer rate, Logarithmic mean temperature difference.

I. INTRODUCTION

A cross flow heat exchanger is one in which two fluids moves in perpendicular to each other. Cross flow heat exchangers are generally used for heat transfer between gas and liquid for both cooling and heating applications. Mahmoud Khaled, et al [1] determined the overall heat transfer coefficient of a cross flow heat exchanger and found an average relative error of 5% were observed. Khitam Fuaad Aefan, et al [2] experimentally studied LMTD was selected to determine the heat transfer rate, over all heat transfer coefficient and effectiveness. Karthik Silaipillayarputhur, et al [3] investigated the steady state sensible performance of multi pass parallel cross flow exchanger, varied capacity rate ratio and ntu. S. D Chavhan, et al [4] compared between elliptical shapes with staggered tube arrangement and circular staggered tube bank arrangement. Circular tubes produce separation, wakes and high-pressure drop. A non-circular tubes offer very low hydraulic resistance and require less pumping power. Chad Randall Harris [5] Studied cross flow micro heat exchanger designed to maximize heat transfer from liquid (water) to gas (air). The cross-flow micro heat exchanger produces a very high heat transfer rate per volume between dissimilar fluids with low fluid pressure drop. Shung wen Kung, et al [6]

describes the interactive effect between the effectiveness and pressure drop and proved that the average temperature of the hot and cold side flow significantly effects the heat transfer rate and pressure drop at same effectiveness. H. Ingimundardottir, et al [7] Studied detection of fouling in a heat exchanger at perfect steady state conditions. To detect fouling when all inputs (inlet temperature of the fluids as well as the mass flow rates) are simultaneously varying. The mass flow rate can vary in a ratio of 2% and inlet temperatures can vary +/- 20%. A.S Krishnan, et al [8] compared conventional staggered flow and double cross flow heat exchanger between heat transfer rate and pressure drop at same conditions for the two configurations. This study reveals that the proposed configuration gives a maximum increase of 27% in heat transfer rate per unit pressure drop. Lubencabezgomez, et al [9] studied thermal performance of multipass parallel cross flow and counter cross flow heat exchangers. Thermal effectiveness of the multipass cross flow configuration varies differently with the number of tube passes. In counter cross flow configuration, the effectiveness increases. The effectiveness alternates in the case of parallel cross flow arrangement though tending progressively to that of the pure parallel flow. Jiangfeng Guo, et al [10] studied matrix analysis indicated that the total heat load of the heat exchanger matrix. When the total heat transfer area and other conditions remain unchanged, the heat load of the heat exchanger matrix enhances as the distributed coordination between the two vectors of the local heat flux density, local heat transfer area improves, and average coordination angle decreases. X.J. LUO [11] Studied cross flow heat exchanger with external and internal recycles. The results shows the dimensionless heat transfer rate rises with the increase of recycle ratio R or Capacitance rate ratio c_2/c_1 or with the decrease of heat transfer area. The maximum increase of efficiency reached up to 28% and 21% for internal and external recycles respectively. Dr. Sadiq Elias Abdullah [12] cross flow heat exchanger with staggered tube bank arrangement studied with four sets of tube banks. Creating a number of (14, 29, 59) V-groove shaped of one mm depth on outer surface of three sets while the fourth remain as it is smooth. The heat transfer rate good for smooth tube banks. Meanwhile other sets show that the heat transfer rate increases with increase of Reynolds number and non-dimensional pressure drop decreases. Abhishek Bhandegaonkar, et al [13]

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Studied the cross-flow heat exchanger with staggered tube bank arrangement with 60° angle of attack is carried out. In heat exchanger thermal hydraulic performance of tubes was calculated by varying mass flow rate of air and its effect on Nusselt number, Reynolds number, Prandtl number, Convective heat transfer coefficient, and friction factor.

Temperature difference between inlet and outlet of air decreases with increase in velocity of air. Tisha Dixit, et al [14] Heat exchanger performance defined in terms of hot and cold fluid effectiveness may have different indications. When both the hot and cold fluids were colder than ambient temperature, the hot fluid effectiveness is inversely proportional to heat in-leak while the cold fluid effectiveness shows direct proportionality to the heat increases. When the ambient thermal resistance is extremely low, the cross flow heat exchanger tends to come in equilibrium with surroundings, when the conductance ratio is high, there is a sharp change in cross flow heat exchanger performance. Tianyi Gao, et al [15] Heat exchangers are important facilities that are widely used in data centers, heating, ventilation and air conditioning systems. The effectiveness of heat exchangers strongly influence the thermal performance of cooling systems. Cheensu An, et al [16] studied thermal hydraulic analysis of cross flow finned tube heat exchanger for an outdoor unit in residential air-conditioning and heat pump applications. An efficient and accurate heat transfer analysis procedure for a multi row cross flow heat exchanger of an air-conditioning system is the steady state 3-dimensional continuity, momentum and energy equations were solved by using the finite volume method to obtain the thermal-hydraulic characteristics of multi row fin and tube heat exchangers. Toolthaisong, et al [17] studied experimentally the effect of attack angles on airside thermal and pressure drop of the cross flow heat exchangers with staggered tube arrangement. The results shows the heat transfer and pressure drop were increased when the attack of angle and aspect ratio increase. Anwar Sadath, et al [18] The heat exchanger tube was modeled as a cantilever beam with two loose baffles/supports, One at the midspan and one at the end. When the amplitude of tube exceeds a certain value, the tube can impact the baffles. This impact force has been modeled either with a cubic spring or a trilinear spring. W.A khan [19] determined an optimal design of tube banks for both inline and staggered arrangements. The results shows staggered arrangement gives a better performance for lower approach velocities and longer tubes. whereas the inline arrangement performs better for higher approach velocities and larger dimensionless pitch ratios. Compact tube banks perform better for both arrangements and for smaller tube diameters. Mansour Nasirikalaji, et al [20] the optimization of cross flow heat exchanger having different tubular routers with and without winglets in cylindrical, square and hexagonal geometries. The optimum Reynolds number range between 2900 and 3750 the heat transfer rate is rather high in cylindrical router with winglet. Reynolds number is around 2750 for the case of hexagonal and square with winglets. The entropy generation rate decreases with increasing Reynolds number.

II. METHODOLOGY

A. Wind tunnel

The schematic diagram of wind tunnel is shown in fig 1. It shows the heat exchanger arrangement with wind tunnel.



Fig 1 Wind tunnel

Wind tunnels are simply hollow tubes at one end and other end rectangular section. They have power full fans that create a flow of air inside the tunnel. Wind tunnels are used to study the gas flow around a body and the forces generated by the gas body interaction, producing a controlled stream of air in order to study the effects of movement through air or resistance to moving air on models of aircraft and other machines and objects. Mostly air is used in wind tunnel. Wind tunnels have been highly lucrative devices for solving design problems in automobiles, boats, trains, bridges and building structures. Wind tunnel create an air velocity ranging from 5m/s to 30m/s.

B. Wind tunnel Specifications

Type: Low speed wind tunnel
Capacity: 30m/s
Max Rpm: 1530
Duty cycle: Continuous

C. Heat exchanger



Fig 2 Heat exchanger(Front view)



Fig 3 (Side view)

A cross flow heat exchanger is one in which the two fluids moves in perpendicular to each other. In cross flow heat exchangers gas flowing over the tubes and liquid flowing inside the tubes. Cross flow heat exchangers are extensively used in the petroleum, petrochemical, air conditioning, food storage, chemical process, thermal power plant, refrigeration, cryogenic, heat recovery and automobile industries.

D. Heat exchanger specifications

Heat exchanger dimensions	
Length	21cm
Width	23cm
Depth	4cm
Tubes inner dia	0.76cm
Tubes outer dia	0.98cm
Tube material	Copper
Shell/frame material	Aluminum

E. Experimental set up with singleheat exchanger

The experimental set up of cross flow heat exchanger is to investigate the heat transfer rate and effectiveness by varying velocity and mass flow rate of fluids. The schematic diagram of cross flow heat exchanger is shown in below fig 4. It consists of a wind tunnel, Heat exchanger, Temperature indicator, Heater, Insulated container. The wind tunnel is a simply hollow tube at one end and other end at rectangular section, create air flow inside of the tunnel with a fan. Heat exchanger is placed inside of the wind tunnel in cross segment zone perpendicular to air stream inside of the wind tunnel. The hot water flows from insulated container to heat exchanger inlet through channel, Circulated in the tubes entire heat exchanger and flowing out side. Analogous air flowing from one end to other inside of the wind tunnel in perpendicular direction of the water flowing inside of the heat exchanger. Heat transfer takes place from hot water flowing inside of the tubes to air flowing over the tubes. The hot water is coming in to the cold water and cold air is getting hotness. To measure air and water temperatures by using temperature indicator sensors. Hot water circulated in the number of tubes inside the heat exchanger is coming in

to cool down by air flowing over the heat exchanger. The water inlet and outlet temperature distinction is more evaluate to air inlet and outlet temperature because of water Circulation and contacting period is more evaluate to air circulating and contacting period is less. Initially experiment is carried at air velocity 15m/s and readings are noted and after the experiment is repeated with different velocities by changing one by one velocity with help of adjustment knob up to 30m/s and readings are noted.

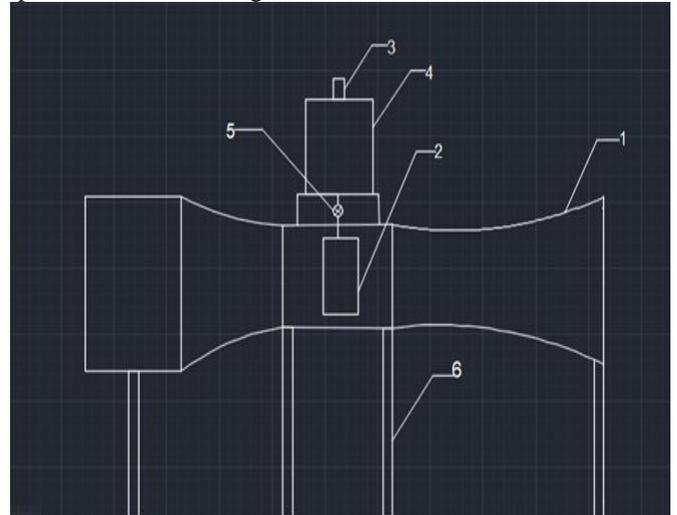


Fig 4 Line diagram of experimental set up

- 1. Wind tunnel 2. Heat exchanger 3. Heater
- 4. Insulated container 5. Control valve 6. Stand



Fig 5 Experimental setup



Fig 6 Cross segment zone

Experimental Study of Heat Transfer Rate in Single and Series Cross Flow Heat Exchanger using Matlab Coding

F. Experimental set up with series heat exchanger(series connection)

The schematic diagram of cross flow heat exchanger with series connection is shown in fig 6. In single heat exchanger we are observed when increase the velocity of air the mass flow rate of air and heat transfer rate increases, at one velocity gives more amount of heat transfer rate, mass flow rate of air and effectiveness. Now again testing with double heat exchanger in series connection examine the heat transfer rate and effectiveness by varying mass flow rate of air and velocity of fluids (air and water) and measure the inlet and outlet temperature of fluids as same as above. Initially experiment carried at air velocity 15m/s with help of a knob on wind tunnel and readings are noted. Then experiment will repeated with different velocities by changing one by one and the readings(inlet and out let temperature of fluids) are noted. Compare to the single heat exchanger with double heat exchanger heat transfer rate, over all heat transfer coefficient, Reynolds number, Nusselt number and effectiveness will increased.



Fig 7 Double heat exchanger (series connection)

III. MATLAB INTRODUCTION

The name MATLAB stand for Matrix Laboratory. MATLAB was written originally to provide easy access to matrix software developed by the LINPACK (linear system package) and EISPACK (Eigen system package) projects. MATLAB is a high performance language for technical computing. It integrates computation, visualization, and it is a modern programming language environment. It has sophisticated data structures, contains built-in editing and debugging tools, and supports object oriented programming. These factors make an excellent tool for teaching and research.

a. MATLAB CODE

```
Tin=input('enter inlet temperature of air in k');
Tout=input('enter outlet temperature of air in k');
tin=input('enter inlet temperature of water in k');
tout=input('enter outlet temperature of water in k');
cph=input('enter specific heat of water in kj/kgk');
cpc=input('enter specific heat of air in kj/kgk');
cf=input('enter correction factor');
a=input('enter cross sectional area in m^2');
```

```
rho=input('enter density of water in kg/m^3');
Rho=input('enter density of air in kg/m^3');
v=input('enter velocity of water in m/s');
V=input('enter velocity of air in m/s');
di=input('enter value of inner diameter in m');
do=input('enter value of outer diameter in m');
ri=input('enter value of inner radius in m');
ro=input('enter value of outer radius in m');
mu=input('enter value dynamic viscosity of water in Ns/m^2');
Mu=input('enter value dynamic viscosity of air in Ns/m^2');
kw=input('enter value of water thermal conductivity in w/mk');
ka=input('enter value of air thermal conductivity in w/mk');
k=input('enter value of material thermal conductivity in w/mk');
c=input('enter value of constant');
m=input('enter value of constant two');
cmin=input('enter value of minimum capacity rate in kj/k');
cmax=input('enter value of maximum capacity rate in kj/k');
pr=input('enter value Prandtle number of water');
Pr=input('enter value Prandtle number of air');
dt2=(tout-Tin);
dt1=(tin-Tout);
lmtd=((dt2-dt1)/(log(dt2/dt1)));
fprintf('value of %d\n',lmtd);
re=((rho*v*di)/mu);
Re=((Rho*V*do)/Mu);
nua=((c)*(re^m)*(pr^0.333));
fprintf('value of %d\n',nua);
Nuw=((0.023)*(Re^0.8)*(Pr^0.4));
fprintf('value of %d\n',Nuw);
hi=((Nuw*kw)/(di));
fprintf('value of %d\n',hi);
ho=((nua*ka)/(do));
fprintf('value of %d\n',ho);
U=(1/(((ro/ri)*(1/hi))+((ro/k)*(log(ro/ri)))+(1/ho)));
fprintf('value of %d\n',U);
ntu=((U*a)/cmin);
fprintf('value of %d\n',ntu);
q=(cf*U*a*lmtd);
fprintf('value of %d\n',q);
C=(cmin/cmax);
e=((1/C)*(1-exp(C-(1-(exp(-ntu))))));
fprintf('value of %d\n',e);
Q=(100:50:400);
ma=(1:0.5:4);
plot(Q,ma)
```

IV. Results and discussion

4.1 Relation between mass flow rate of air (m_a) and heat transfer rate (Q) at single heat exchanger

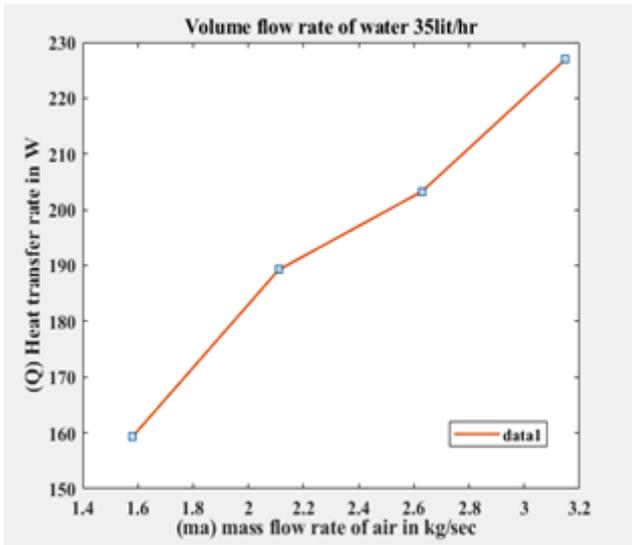


Fig 4.1.1 Graph between m_a and Q at volume flow rate of water 35lit/hr

Fig 8 represents the graph between m_a and Q at water volume flow rate is 35lit/hr. In this heat transfer rate is directly proportional to mass flow rate of air as a result mass flow rate of air increases corresponding heat transfer rate increases. Because mass flow rate of air, Reynolds number increased when increases the velocity of air. That will increase the amount of air used to be in contact with the heat exchanger surface to reduce the heat. The maximum and minimum amount of heat transfer rate is 227w and 159w corresponding air velocity 30m/sec and 15m/sec.

4.2 Relation between mass flow rate of air (m_a) and heat transfer rate (Q) at single heat exchanger

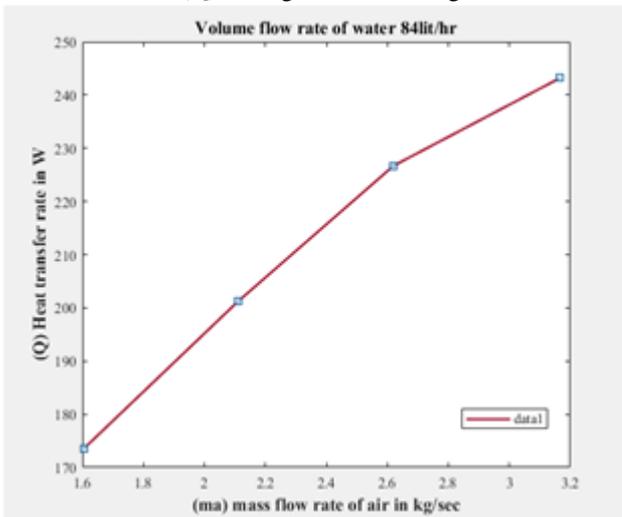


Fig 4.2.1 Graph between m_a and Q at volume flow rate of water 84lit/hr

Fig 4.2.1 represents the graph between m_a and Q at water volume flow rate is 84lit/hr. In this heat transfer rate is depends on the mass flow rate of air, heat transfer rate increases when mass flow rate of air increases and corresponding Reynolds number is also increased. Compare to the fig 8 here the amount of water volume flow rate

increased then difference between inlet and outlet temperature of fluids is also increased. The maximum and minimum amount of heat transfer rate is 243w and 173w at corresponding air velocities 30m/sec and 15m/sec.

4.3 Relation between mass flow rate of air (m_a) and heat transfer rate (Q) at series heat exchanger

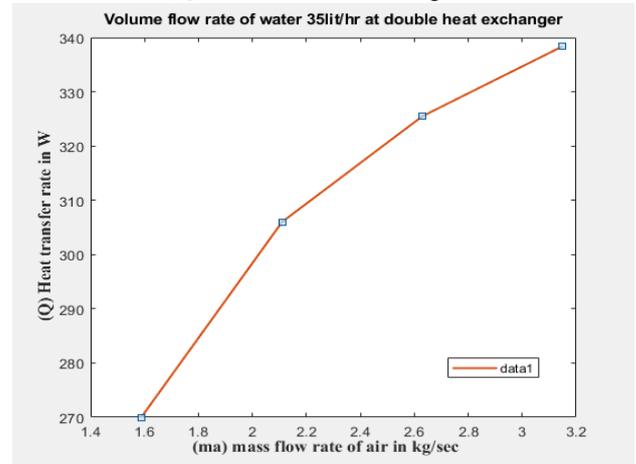


Fig 4.3.1 Graph between m_a and Q at volume flow rate of water 35lit/hr at series heat exchanger

Fig 4.3.1 signifies the volume flow rate of water is 35lit/hr at series heat exchanger in series connection. Heat transfer rate is directly proportional to mass flow rate of air so mass flow rate of air increases corresponding heat transfer rate increases. Because mass flow rate of air, Reynolds number increased when increases the velocity of air, the amount of air used to be contact with the heat exchanger surface to reduce heat. The maximum and minimum amount of heat transfer rate is 338w and 270w at series heat exchanger and in single heat exchanger is 227w and 159w at equivalent air velocities 30m/sec and 15m/sec. Compare to the series heat exchanger and single heat exchanger at same water volume flow rate, the amount of heat transfer rate increased is 48.8% and 69.8% of heat transfer rate in series heat exchanger analogous air velocities 30m/sec and 15m/sec.

1.4 Relation between mass flow rate of air (m_a) and heat transfer rate (Q) at double heat exchanger (series connection)

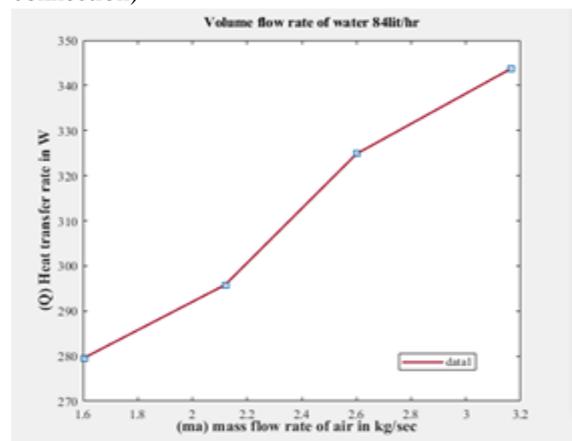


Fig 4.4.1 Graph between m_a and Q at volume flow rate of water 84lit/hr at series heat exchanger

Experimental Study of Heat Transfer Rate in Single and Series Cross Flow Heat Exchanger using Matlab Coding

Fig 11 denotes the graph between ma and Q at volume flow rate of water is 84lit/hr at double heat exchanger in series connection. Mass flow rate of air directly proportional heat transfer rate hence heat transfer rate increases when mass flow rate of air increased. The maximum and minimum amount of heat transfer rate is 343w and 279wat series heat exchanger and in single heat exchanger is 243w and 173w resultant air velocities 30m/sec and 15m/sec. Compare to the single heat exchanger and series heat exchanger the amount of heat transfer rate increases is 41.5% and 61.27% in series heat exchanger at corresponding air velocities 30m/sec and 15m/sec.

1.5 Relation between velocity of air and LMTD,NU,H,U at volume flow rate of water 35lit/hr

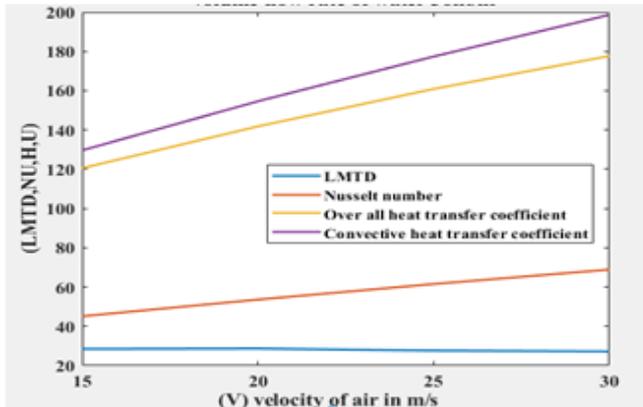


Fig 4.5.1 Variation of velocity of air (V_a) with LMTD, Nu, h, U

The above graph indicates the variation of velocity of air (V_a) with logarithmic mean temperature difference (LMTD), Nusselt number (Nu), Convective heat transfer coefficient (h), Over all heat transfer coefficient (U) at volume flow rate of water 35 lit/hr. It is observed that the Velocity of air directly proportional to Nusselt number, convective heat transfer coefficient, overall heat transfer coefficient and in-directly proportional to LMTD so velocity of air increases analogous Nusselt number, convective heat transfer coefficient and over all heat transfer coefficient increases and logarithmic mean temperature difference slightly decreases. The air velocity varies from 15m/sec to 30m/sec when Nu, h, U increases heat transfer rate(Q) is also increases.

1.6 Relation between velocity of air (V_a) and LMTD, Nu, h, U

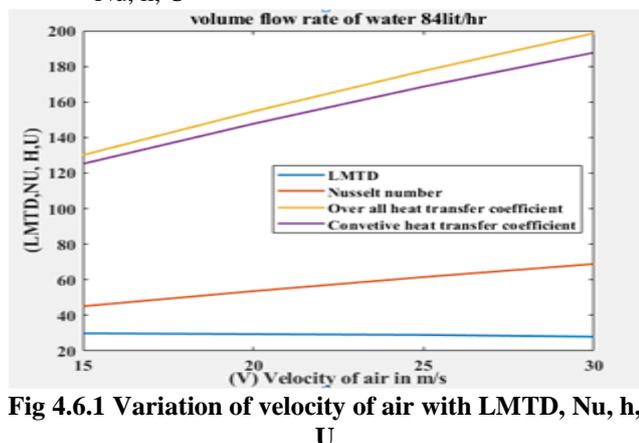


Fig 4.6.1 Variation of velocity of air with LMTD, Nu, h, U

Fig 4.6.1 It shows the variation of velocity air (V_a) with logarithmic mean temperature difference (LMTD), Nusselt

number (Nu), convective heat transfer coefficient (h), over all heat transfer coefficient (U) at volume flow rate of water 84 lit/hr. It is observed that the velocity of air directly proportional to Nusselt number, convective heat transfer coefficient and over all heat transfer coefficient and incidentally proportional to logarithmic mean temperature difference method so velocity of air increases corresponding Nu, h, U increases and LMTD slightly decreases. Velocity of air varies from 15m/sec to 30m/sec when V_a increases equivalent Nu, h, U increases and heat transfer rate (Q) is also increased.

4.7 Heat transfer rate and mass flow rate of air at different velocities at single and series cross flow heat exchanger.

S.N	Velocity (m/s)	Mass flow rate of air(kg/s)	Heat transfer rate (kw) at single heat exchanger	Heat transfer rate (kw) at double heat exchanger	Increased % of heat transferrate at doublehe at exchanger
1.	15 m/s	1.604	173.59	279.59	61.27%
2.	20 m/s	2.11	201.20	295.40	46.76%
3.	25 m/s	2.62	226.67	324.87	43.36%
4.	30 m/s	3.16	243.23	343.93	41.15%

V. CONCLUSION

The cross-flow heat exchangers are used to transfer thermal energy from hot fluid to cold fluid has been studied theoretically and experimentally. Cross flow heat exchangers are generally used for heat transfer between a gas and liquid for both heating and cooling process. The most common examples of cross flow heat exchanger is condenser, radiator and evaporative coil. LMTD(logarithmic mean effective temperature difference) method is used to determine the heat transfer rate, overall heat transfer coefficient and effectiveness. The resultsshow the heat transfer rate increases when the mass flow rate of air increases.

- Flow velocity of the working fluid is effective on the efficiency of heat exchanger.
- Increasing water velocity enhance the heat transfer rate and reduces the irreversibility.
- For heat transfer enhancement increasing heat transfer area, enhancing the turbulence and reducing boundary layer thickness and generating the secondary flow.
- Compare to the single heat exchanger with series heat exchanger at volume flow rate of water 35lit/hr. The amount of heat transfer rate increased in series heat exchanger is 69.8% and 48.8% at resultant air velocities 15m/s and 30m/s.
- Compare to the single heat exchanger with series heat exchanger at volume flow rate of water 84lit/hr. The amount of heat transfer rate increased is 61.2% and 41.5% in series heat exchanger at analogous air velocities 15m/s and 30m/s.

- When we increased velocity of air corresponding mass flow rate of air, Reynolds number, Nusselt number, convective heat transfer coefficient and over all heat transfer coefficient automatically increases.

II. NOMENCLATURE

T_{hi} = Temperature of water at inlet in k
 T_{ho} = Temperature of water at outlet in k
 T_{ci} = Temperature of air at inlet in k
 T_{co} = Temperature of air at outlet in k
 LMTD = logarithmic mean temperature difference
 R = Capacity ratio without units
 ϵ = Effectiveness without units
 A = Surface area in m^2
 m_w = mass flow rate of water in kg/sec
 m_a = mass flow rate of air in kg/sec
 V_a = velocity of air in m/sec
 V_w = velocity of water in m/sec
 Re = Reynolds number
 Nu = Nusselt number
 h_i = Convective heat transfer coefficient at in side in w/m^2k
 h_o = Convective heat transfer coefficient at outside in w/m^2k
 U = Over all heat transfer coefficient in w/m^2k
 ntu = number of transfer units
 F = Correction factor
 Q = Heat transfer rate in w
 μ = dynamic viscosity in Ns/m^2
 ρ = Density in kg/m^3
 C_{min} = minimum heat capacity
 C_{max} = maximum heat capacity
 C = capacity ratio
 Subscripts
 i = inlet
 o = outlet
 a = air
 w = water
 min = minimum
 max = maximum

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